



VIT

Vellore Institute of Technology
(Deemed to be University under section 3 of U.C.C. Act 1996)

SCHOOL OF CHEMICAL ENGINEERING
CONTINUOUS ASSESSMENT TEST -II
FALL SEMESTER 2025-2026

SLOT: A1+TA1+TAA1

Programme Name & Branch	: B.Tech - Chemical	
Course Code	: BACHE101	
Course Name	: Chemical Engineering Thermodynamics - TH	
Faculty Name(s)	: L.Muruganandam	
Class Number(s)	: VL2025260107117	
Date of Examination	: 05/10/2025	
Exam Duration	: 90 minutes	Maximum Marks: 50

General instruction(s): Read carefully the statement and answer all Questions.

Q. No	Question	M												
1.	A high-pressure gas compressor operates with methane (CH₄) at 200 K. At this temperature, the gas is highly non-ideal. The volumetric data for methane vapor can be accurately represented by the truncated virial equation of state (up to the second term): $\frac{PV}{RT} = 1 + \frac{B}{V}$ where Z is the compressibility factor, and B is the second virial coefficient. The experimental data for methane at 200 K yields the following values: Gas Constant, R = 8.314×10⁻⁵ m³·bar/(mol·K) Second Virial Coefficient, B = -4.00 × 10⁻⁵ m³/mol. Calculate the fugacity (f) of methane at a pressure of 50 bar and 200 K.	10												
2.	A 30% mole fraction ethanol (EtOH) and water (H₂O) solution is to be prepared. You need to produce a final volume of 500 mL (V_{sol} = 0.0005 m³) of the mixture. Use the following data for the components at the given conditions: <table><thead><tr><th>Component</th><th>Mole Fraction</th><th>Pure Molar Volume m³/mol</th><th>Partial Molar Volume in 30% solution m³/mol</th></tr></thead><tbody><tr><td>Ethanol (E)</td><td>0.3</td><td>58.0×10⁻⁶</td><td>55.0×10⁻⁶</td></tr><tr><td>Water (W)</td><td>0.7</td><td>18.0×10⁻⁶</td><td>17.5×10⁻⁶</td></tr></tbody></table>	Component	Mole Fraction	Pure Molar Volume m ³ /mol	Partial Molar Volume in 30% solution m ³ /mol	Ethanol (E)	0.3	58.0×10 ⁻⁶	55.0×10 ⁻⁶	Water (W)	0.7	18.0×10 ⁻⁶	17.5×10 ⁻⁶	10
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3.	For a mixture of acetic acid and toluene containing 0.46 mole fraction toluene, the partial pressure of acetic acid and toluene are found to be 0.12 bar and 0.17 bar respectively at 340 K. The vapour pressure of pure components at this temperature are 0.26 bar and 0.19 bar for toluene and acetic acid respectively. The Henry's law constant for acetic acid is 0.55 bar. Calculate the activity and activity coefficient for acetic acid in the mixture (a) Based on Lewis–Randall rule (5) (b) Based on Henry's law(5)	10												



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4.	(i)What contributes to the non-ideal behaviour of the solution. (3) (ii)Calculate the available degrees of freedom for the given non-reacting system: A vapour phase containing ammonia in air and a liquid phase containing ammonia in water at a specified temperature.(2) (iii)Why does the boiling point diagram at a higher pressure lie above that at a lower pressure?(2) (iv)How would you calculate the constant pressure y-x data of a binary mixture using an average value of the relative volatility? (2)	10												
5.	For the system n-pentane (1)-n-heptane (2), the vapour pressures are given by the Antoine Equation $\ln P = A - \frac{B}{T - C}$ where P is in kPa and T is in K. The constants are as follows. <table><tr><th>System</th><th>A</th><th>B</th><th>C</th></tr><tr><td>n-Pentane</td><td>13.8183</td><td>2477.07</td><td>40.00</td></tr><tr><td>n-Heptane</td><td>13.8587</td><td>2911.32</td><td>56.56</td></tr></table> Assuming that the solution formed is ideal, calculate: (a) The composition of the liquid and vapour in equilibrium at 95 kPa and 336.2 K. (5) (b) The composition of the vapour in equilibrium with a liquid containing 34% (mol) pentane and the equilibrium temperature at $P = 95$ kPa. (5)	System	A	B	C	n -Pentane	13.8183	2477.07	40.00	n -Heptane	13.8587	2911.32	56.56	10
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